

# intro.pid Introducing PID control

1 One of the most ubiquitous types is the **proportional-integral-derivative** (PID) controller. It has a transfer function with real constants  $K_P$ ,  $K_I$ , and  $K_D$ :

**PID controller**

$$C(s) = \underbrace{K_P}_{\text{proportional}} + \underbrace{K_I/s}_{\text{integral}} + \underbrace{K_D s}_{\text{derivative}} . \quad (1)$$

Remember: the controller operates on the error  $E(s)$ , so the PID controller effectively sums terms proportional to the error, its integral, and its derivative. Inspecting this in the time domain with error  $e(t)$  by taking the inverse Laplace transform of the output  $U(s) = C(s)E(s)$ ,

$$u(t) = \underbrace{K_P e(t)}_{\text{proportional}} + K_I \underbrace{\int_0^t e(\theta) d\theta}_{\text{integral}} + \underbrace{K_D \dot{e}(t)}_{\text{derivative}} . \quad (2)$$

2 So the control effort  $u$  is responsive to:

- P** the amount and direction of error (reactive, spring-like),
- I** the accumulation of error over time (memoried, mass-like), and
- D** the time rate of change of the error (anticipatory, damper-like).

Although the mechanical spring-mass-damper analog above has its limitations, it is helpful for our intuition. More generally, we can consider the three constants  $K_P$ ,  $K_I$ , and  $K_D$  to be “knobs” with which we can include more or less of each term.

3 Just how a controller will affect the closed-loop response is significantly dependent on the *plant* dynamics. Therefore, there is no way to make fully general statements about the impact of each of the PID terms. This is why we need the detailed analytic design tools of [Chapter rldesign](#) and the intervening chapters hence. However, for some simple systems, we can make the assertions of [Table pid.1](#).

4 There are many methods of **tuning** a PID controller: selecting  $K_P$ ,  $K_I$ , and  $K_D$  to meet certain performance criteria. The **root locus**

**Table pid.1:** occasionally true generalities about PID controller terms.

Proportional	Integral	Derivative
<ul style="list-style-type: none"> <li>• is the workhorse</li> <li>• speeds up responses</li> <li>• can lead to instability when too large</li> </ul>	<ul style="list-style-type: none"> <li>• improves or eliminates steady-state error</li> <li>• slows down the response</li> <li>• becomes a liability when it can't forget (integral windup)</li> </ul>	<ul style="list-style-type: none"> <li>• speeds up the response</li> <li>• can yield jitter when measurement noise is large</li> <li>• can lead to instability when measurement noise is large</li> </ul>

**tuning**

**root locus**

design method of [Chapter rldesign](#) and the **frequency response** design method of [Chapter freqd](#) allow us to precisely design for specific performance criteria. However, there are times when specific performance criteria and involved analysis are not available or convenient. In these cases, hand-tuning is possible via several algorithms. One such algorithm is presented in the following section.

**frequency response**

**Ziegler–Nichols tuning method**

5 The Ziegler–Nichols method of tuning a PID controller is presented in the following algorithm.

1. Set  $K_P, K_I, K_D = 0$ .
2. Increase  $K_P$  until a marginally stable response<sup>1</sup> is observed.
3. Record this **ultimate gain**  $K_u$  and the **oscillation period**  $T_u$ .
4. Set the controller gains:

1. This can be the impulse, step, or free response. Furthermore, it can be oscillatory.

**ultimate gain**  $K_u$   
**oscillation period**  $T_u$

$$K_P = 0.6K_u \quad K_I = 1.2K_u/T_u \quad K_D = 3K_uT_u/40. \tag{3}$$

**Example intro.pid-1**

For the block diagram of [Fig. pid.1](#), with the plant

$$G(s) = \frac{15000}{s^4 + 50s^3 + 875s^2 + 6250s + 15000}$$

use the Ziegler–Nichols method to design a PID controller  $C(s)$ .

We proceed with Matlab, symbolically at first.

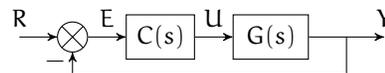
Let's define the transfer functions.

```
syms S kp ki kd % S is the laplace transform s
G_sym = 15000/(S^4+50*S^3+875*S^2+6250*S+15000); % plant
C_sym = kp + ki/S + kd*S; % PID controller transfer fun
```

From the preceding lecture's ??, the closed-loop transfer function is as follows.

```
CL_sym = simplify( ...
```

**re: hand-tuning a PID controller**



**Figure pid.1:** block diagram for [Example intro.pid-1](#).

```
C_sym*G_sym/(1+C_sym*G_sym) ...
)
```

```
CL_sym =
```

```
(15000*kd*S^2 + 15000*kp*S + 15000*ki)/(15000*S +
↪ 15000*ki + 15000*S*kp + 15000*S^2*kd + 6250*S^2
↪ + 875*S^3 + 50*S^4 + S^5)
```

I have created a function `sym_to_tf` that creates a `tf` object, which we'll need for simulation.<sup>a</sup>

```
type sym_to_tf.m
```

```
function tf_obj = sym_to_tf(sym_tf,s_var)
% TODO test to make sure s_var is in
↪ symvar(sym_tf) ...
syms(symvar(sym_tf))
syms s
sym_tf = subs(sym_tf,s_var,s);
tf_str = char(sym_tf);
s = tf([1,0],[1]);
eval(['tf_obj = ',tf_str,'];)
```

Let's wrap it in a function of our own `K_sub`, which will create a closed-loop `tf` object from our `CL_sym` with the PID gains included.

```
K_sub = @(Kp,Ki,Kd) sym_to_tf( ...
    subs( ...
        CL_sym, ...
        {kp,ki,kd}, ...
        {Kp,Ki,Kd} ...
    ), ...
    S ...
);
K_sub(1,0,0) % e.g.
```

```
ans =
```

```

          15000 s
-----
s^5 + 50 s^4 + 875 s^3 + 6250 s^2 + 30000 s
```

```
Continuous-time transfer function.
```

Now let's use `impulse` to simulate the response starting with a small proportional gain.

```
[y,t] = impulse(K_sub(1,0,0));
```

Now, we should plot the result – see Fig. pid.2.

```
figure
plot(t,y)
grid on
xlabel('time (s)')
ylabel('impulse response')
```

If we iteratively increase  $K_p = 1 \rightarrow 3 \rightarrow 5.25$  (the response for each of these values is plotted in Fig. pid.3), we find that around the last value, the system becomes marginally stable and therefore

$$K_u = 5.25. \tag{4}$$

The oscillation period appears to be around  $T_u = 0.56$  seconds. Defining these quantities, we can now compute  $K_I$  and  $K_D$  from Eq. 3.

```
Ku = 5.25;
Tu = 0.56;
Kp = 0.6*Ku;
KI = 1.2*Ku/Tu;
KD = 3*Ku*Tu/40;
disp(sprintf('KP = %0.2f, KI = %0.2f, KD = %0.2f', ...
    KP, KI, KD ...
))
```

KP = 3.15, KI = 11.25, KD = 0.22

Let's try out this controller for step response and see how it looks.

```
[y,t] = step(K_sub(KP,KI,KD));
figure
plot(t,y)
xlabel('time (s)')
ylabel('step response')
```

The resulting step response is plotted in Fig. pid.4. We didn't have specific expectations for performance, here, but this result is a nice, average-looking step response with some overshoot and a decent settling time.

a. The function is available in the repo: [github.com/ricopicone/matlab-rico](https://github.com/ricopicone/matlab-rico).

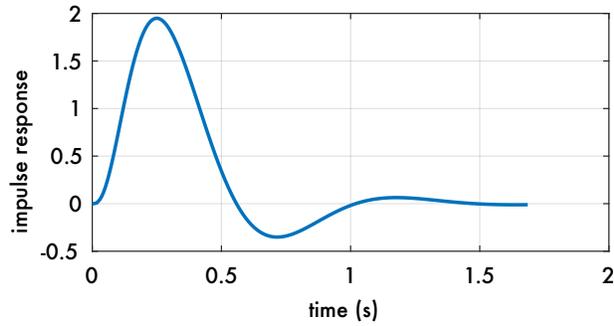


Figure pid.2: impulse response with (small)  $K_p = 1$ .

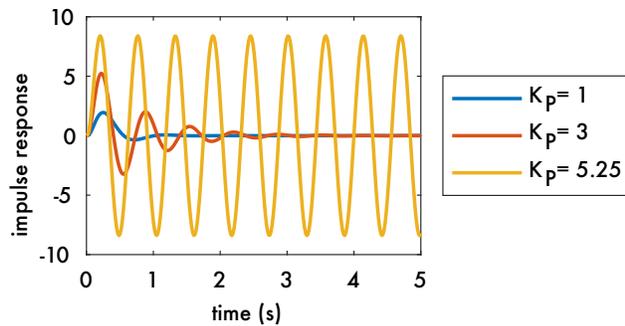


Figure pid.3: impulse responses with  $K_I = K_D = 0$  and  $K_p$  as shown.

